

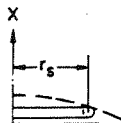
# Predicting Flow Induced Vibration

in II Road Regions of Heat Ex

degenerate An Engineering Solution

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It is now generally recognized that the liquid flow induced vibrations are



$2r_s$

(a) SLOTTED  
BAFFLE

(b) SOLID  
BAFFLE

FIG. 3. Double segmental baffle shapes.



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$R$  is the outer bundle radius,  $\eta$  is the perforation coefficient of the bundle surface defined as

$$\eta = \frac{p-d}{\pi} \quad (11)$$

where  $p$  and  $d$  are the transverse tube pitch and tube O.D. respectively.

the surface area of a semi-circular cylinder of radius  $r_s$ , and length  $2(R_s - x')$ , where  $R_s$  denotes the inside radius of the shell. Substituting for  $a$  from Eq. (9)

where

$$\xi = \frac{R_s}{r} \quad (22)$$

$\xi$  is close to 1 for most practical designs. Equation (21) determines  $C$ . The velocity profile follows from Eq. (9), which cast in a more direct form below.

$$q = \frac{C}{\left[ 1 - \frac{\omega \chi (N-1)}{1 - \omega} \right]^{1/2}} \quad (23)$$

where  $q$  is the volumetric flow rate through a stratum of unit width, and outer radius  $y$ . Hence, the velocity  $V(y, r)$  at bend radius  $r$  in the stratum of outer radius  $y$  is given by

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Equation (9.2) will be a good one if a lower bound for  $\beta$  since the expressions





In terms of  $S$ , the vortex shedding frequency is given by

$$f = \frac{SV}{d} \quad (35)$$

where  $V$  is the corresponding flow velocity and  $d$  is outside tube diameter. The

flow velocity at  $R = 11.8$  in. is found to be 70.1 in./sec. Hence Eq. (35) yields

*Predicting Flow Induced Vibration in U-Bend Regions of Heat Exchangers*

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